

Fluorine Substitution in Diamine Covalent Organic Frameworks: Computational Analysis of CO₂/N₂ Adsorption and Permeability

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Abstract

In this study, we investigated the effect of fluorine substitution on a previously reported diamine-based covalent organic framework (COF), designated as IPB-2H. A new fluorinated analogue namely IPB-2F2 was modeled and its adsorption and permeability characteristics for CO₂/N₂ gas mixtures were evaluated through computational analysis. Ab initio structural optimization results showed that the reduced pore size of IPB-2F2 compared to IPB-2H was attributed to the larger atomic size and higher electronegativity of fluorine compared to hydrogen atom. Molecular dynamics (MD) simulations demonstrated that IPB-2F2 exhibited lower permeation rates for CO₂ and N₂ than its non-fluorinated counterpart; indicating that fluorine atoms effectively reduced gas permeation. Adsorption isotherms revealed enhanced adsorption capacities for IPB-2F2, with increased CO₂ affinity resulting from strong van der Waals interactions. Selectivity analyses showed that IPB-2F2 preferentially absorbed CO₂ over N₂, with selectivity values consistently greater than 1. The enhanced gas uptake capacity and hydrophobicity of IPB-2F2 highlighted its potential for industrial applications as a post-combustion CO₂ capture material.

Keywords

Adsorption, Computational, CO₂ Capture, Permeability

Received: 19 July 2024, Accepted: 18 September 2024

<https://doi.org/10.26554/sti.2025.10.1.18-26>

1. INTRODUCTION

The need for effective CO₂ capture and storage (CCS) technologies has become increasingly critical in the face of escalating greenhouse gas emissions, mitigating environmental pollution and global climate change (Dziejarski et al., 2023; Ghiat and Al-Ansari, 2021). CCS involves capturing CO₂ emissions from industrial processes and power plants, transporting to storage sites, and sequestering to prevent the release of CO₂ into the atmosphere (Hanifa et al., 2023). A major obstacle in this field is the development of materials that selectively and efficiently captured CO₂ from gas mixtures, such as post-combustion flue gas, which predominantly consists of N₂ gas (Gambelli et al., 2021).

High regeneration costs, low selectivity, and stability issues are often encountered with current materials used for CO₂ capture, such as amine-based solvents and zeolites (Boer et al., 2023; Hanifa et al., 2023). Amine scrubbing, for instance, is widely used but is energy-intensive and suffers from degradation over time (Hanifa et al., 2023; Yoro et al., 2021). While zeolites often lack the necessary selectivity for CO₂ over N₂

molecules (Boer et al., 2023; Ganesan and Shaijumon, 2016). Metal-organic frameworks (MOFs) have shown promise due to their tunable pore structures and functionalization capabilities, yet their practical application is sometimes hindered by stability issues (Feng et al., 2020; Yuan et al., 2018). Covalent organic frameworks (COFs) have emerged as promising candidates in this regard due to their tunable porosity, high surface area, lightweight, and structural versatility (Liang et al., 2020; Zhao et al., 2018). These characteristics enable COFs to be designed with specific pore sizes and functional groups that enhance their attractive interactions towards CO₂ molecules, making them highly effective as selective adsorbents.

Fluorine substitution in adsorbing materials is a burgeoning area of research due to the potential enhancement in gas adsorption and separation properties. Fluorination has been shown to significantly alter the chemical and physical properties of materials, including increased hydrophobicity, enhanced thermal stability, and modified electronic properties (Liu et al., 2019). Fluorinated MOFs have been shown to enhance gas sorption due to the strong electrostatic interactions of certain gas molecules within the pore walls of porous materials

(Amooghin et al., 2022). Moghadam et al. (2017) have synthesized F-MOF-1 with the highest uptake of CO₂, which is 11.0 mol L⁻¹ at 298 K and 55 bar and has strong hydrophobic properties. D'Amato et al. (2019), Chernikova et al. (2020), and Venturi et al. (2022) also report improved CO₂ capture performance and selectivity in fluorinated MOFs.

In our previously published study (Apriliyanto et al., 2020), we explored the adsorption sites and adsorption energies of CO₂ and N₂ molecules on 2D-COFs constructed from 1,3,5-tris(chloromethyl)benzene based building units and diamine based linkers (e.g. IPB-2H) using a combination of density functional theory (DFT) calculations and molecular dynamics (MD) simulations. Our findings demonstrated the competitive nature of these COFs with other 2D materials for carbon capture and separation applications, showcasing their efficient and rapid separation and adsorption capabilities. Based on our previous results, in this paper we focused on the computational analysis regarding CO₂/N₂ adsorption and permeability properties of fluorinated COFs. Specifically, we investigated the impact of substituting hydrogen with fluorine atoms in the benzene units of our previously reported COF (IPB-2H) producing a new fluorinated analogue structure, which designated as IPB-2F2 (Figure 1). This modification is expected to improve CO₂ adsorption capacity and selectivity, due to the distinctive electronic and steric effects introduced by the fluorine atoms. Our study employs advanced computational techniques to provide a detailed understanding of the intermolecular interactions and adsorption dynamics within these fluorinated COFs.

2. EXPERIMENTAL SECTION

2.1 Structural Modeling

The smallest unit cell of the IPB-2F2 COF determined via the topological approach was optimized for its structure and lattice parameters using ab initio methods employing the periodic DFT calculations using the Quantum ESPRESSO package (Giannozzi et al., 2017). The periodic model was constructed with initial supercell lattice parameters and sufficient vacuum space to prevent undesired interactions between layers along the *z*-axis. This supercell model adopted a hexagonal Bravais lattice configuration, comprising 78 atoms in total. Periodic DFT relaxations were conducted using the generalized gradient approximation (GGA) of Perdew-Burke-Ernzerhof (PBE) method. The projector augmented wave (PAW) pseudopotentials and an energy cutoff of 700 eV with 5 × 5 × 1 Monkhorst-Pack *k*-points were implemented for the geometry optimizations (Bartolomei and Giorgi, 2016). After obtaining the optimum structure, the charge of each atom was calculated through single point DFT calculations using the B3LYP hybrid functional and RIJCOSX approximation with def2-TZVP basis. The partial atomic charge was then obtained through Hirshfeld analysis implemented in the ORCA quantum chemistry program (Neese et al., 2009).

2.2 Molecular Dynamics (MD) Simulations

In this study, MD simulations were conducted inside a 90.18 × 78.09 × 179.49 Å³ simulation box in the canonical ensemble (NVT) with periodic boundary conditions (PBC) by using the DL_POLY program (Smith et al., 2005). Simulations were performed at 353 K (a typical temperature of post-combustion flue gas) employing the Nose-Hoover thermostat with a 0.5 ps relaxation constant for systems composing of CO₂/N₂ gas mixture with ratio of 1:1 (Goethem et al., 2024). Pressure variation (1.00, 2.54, 3.18, 4.00, and 5.47 atm) was carried out by varying the amount of gas molecules using the Peng-Robinson equation of state. The IPB-2F2 and gas molecules were modelled as rigid bodies approach, thus only non-covalent interactions, i.e. electrostatic and non-electrostatic (van der Waals), were contributed to the total energies. A 15 Å cut-off distance was applied for both non-electrostatic and electrostatic interactions, in which the electrostatic contributions were computed via Ewald method and the non-electrostatic interactions via Improved Lennard-Jones (ILJ) potential (Apriliyanto et al., 2024). MD simulations lasted for 6 ns, including a 0.5 ns thermal equilibration, with a 1 fs time step. Trajectory data were then recorded every 2 ps and analyzed to determine permeation rate and adsorption isotherm.

3. RESULT AND DISCUSSION

3.1 IPB-2F2 COF Structure

COFs are nanoporous organic materials composed of periodically repeating units connected by covalent bonds, offering advantages such as low density, customizable pore size and structure, high thermal stability, and large surface area due to their light-element composition and strong covalent bonds (Feng et al., 2012; Huang et al., 2015). COFs have uniform pore sizes and can be tailored for various functions, enhancing their applicability in gas separation (Kumar et al., 2022; Liu et al., 2021). Herein, we proposed a novel fluorinated COF, denoted as IPB-2F2, that was newly designed from our previously reported IPB-2H structure (Apriliyanto et al., 2022) through the incorporation of fluorine atoms into the linker (Figure 2).

Structure optimization of IPB-2F2 was successfully performed using periodic DFT method within the PBE/PAW approach. The optimized structure of IPB-2F2 was evaluated by comparing it with the original COF structure (i.e. IPB-2H) to assess the impact of fluorine addition. IPB-2F2 exhibited a hexagonal lattice with optimized lattice parameters for *a* and *b* of 22.545 Å (Figure 2(a)), consistent with the hexagonal lattice vector angle of 120° and aligning with our previous results. In addition to the optimized lattice parameters, the optimized structural parameters in terms of bond radius and bond angle were benchmarked with other comparable structures. The optimized structural parameters are shown in the Table 1. Based on the results reported in Table 1, IPB-2F2 exhibits bond lengths and angles that are generally consistent with those of IPB-2H and some existing literatures. However, some deviations are present as consequences of strong fluorine electronegativity,

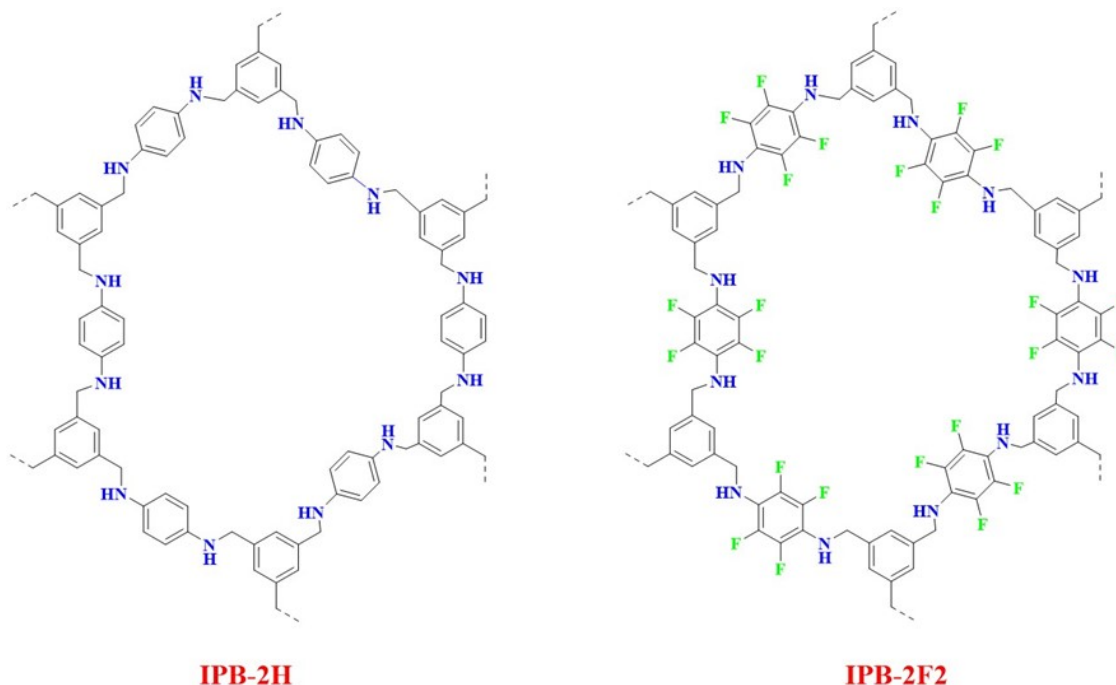


Figure 1. Two Dimensional (2D)-COFs Structures of IPB-2H (Apriliyanto et al., 2022) and IPB-2F2 (This Work)

which can redistribute electron density within molecules affecting their molecular geometry (Pilia et al., 2018).

Before conducting MD simulations, the partial charges of each atom in IPB-2F2 COF were determined to study the electrostatic interactions between CO_2/N_2 gas mixture and COF (Tong et al., 2016). Partial atomic charge parameters for a unit cell of IPB-2F2 were calculated using DFT method at B3LYP/def2-TZVP level, and these values were compared with those of IPB-2H. The pore size of IPB-2F2 COF shown in Figure 2(b) was estimated based on electron density method, yielded an effective pore size of 14.839 Å; which was smaller than 15.167 Å reported for IPB-2H. The reduction in pore size is attributed to the larger atomic size and higher electronegativity of fluorine atoms compared to hydrogen atoms, consistent with findings reported by Zhao et al. (2013) that fluorinated covalent triazine-based frameworks (CTFs) have smaller pore sizes (< 0.50 nm) compared to non-fluorinated CTFs.

3.2 Molecular Dynamics (MD) Simulations Results

MD simulations were conducted to investigate the interactions between the IPB-2F2 membrane and CO_2/N_2 gas mixture at 353 K, simulating post-combustion conditions. The optimized IPB-2F2 membrane with a size of $90.18 \times 78.09 \text{ \AA}^2$ was placed in the center of the simulation box (Figure 3), where CO_2 and N_2 molecules were randomly placed according to predetermined pressure variations. In this study, we consider CO_2/N_2 mixture to model flue gas where nitrogen gas always limits the CO_2 uptake capacity of a material. Moreover, we choose the gas ratio to be 1:1 to study the competitive intermolecular interactions between CO_2 -COF and N_2 -COF as an

equal fraction. Therefore, the gas uptake capacity and selectivity of the materials can be measured fairly without domination of a certain gas molecule.

The IPB-2F2 as well as the CO_2 and N_2 gas molecules were treated as rigid structures during the MD simulations. At the time of simulations, thermal equilibration was first carried out for 0.5 ns followed by simulation and calculation of intermolecular interactions for 5.5 ns. Trajectory data and simulation results were compiled every 2 ps, so that about 3000 frames were obtained from each performed simulation. Several parameters were evaluated to assess the performance of the IPB-2F2 membrane compared to IPB-2H; including permeability, adsorption capacity, and selectivity. The permeance value for each gas was obtained from the slope of the permeation rate line against pressure (Figure 4, left panel). At identical pressures, the permeation rates of CO_2 and N_2 molecules for IPB-2F2 are lower than those reported for IPB-2H. This indicates that the addition of fluorine atoms can restrain the permeation rate of gas molecules, particularly CO_2 . Yan et al. (2019) suggest that the high electronegativity of fluorine atoms enhances the affinity for CO_2 molecules, thereby increasing CO_2 adsorption and decreasing CO_2 permeation for the fluorinated COFs membrane.

Figure 4 (left panel) shows that CO_2 permeance value is higher than N_2 molecules. This is due to the attraction of IPB-2F2 towards CO_2 gas molecules is stronger than N_2 . Figure 4 right panel, illustrates the adsorption isotherm curves, showing the average adsorbed gas per surface area unit of membrane against the applied pressure for both IPB-2F2 and IPB-2H COFs. The stronger affinity for CO_2 molecules is also

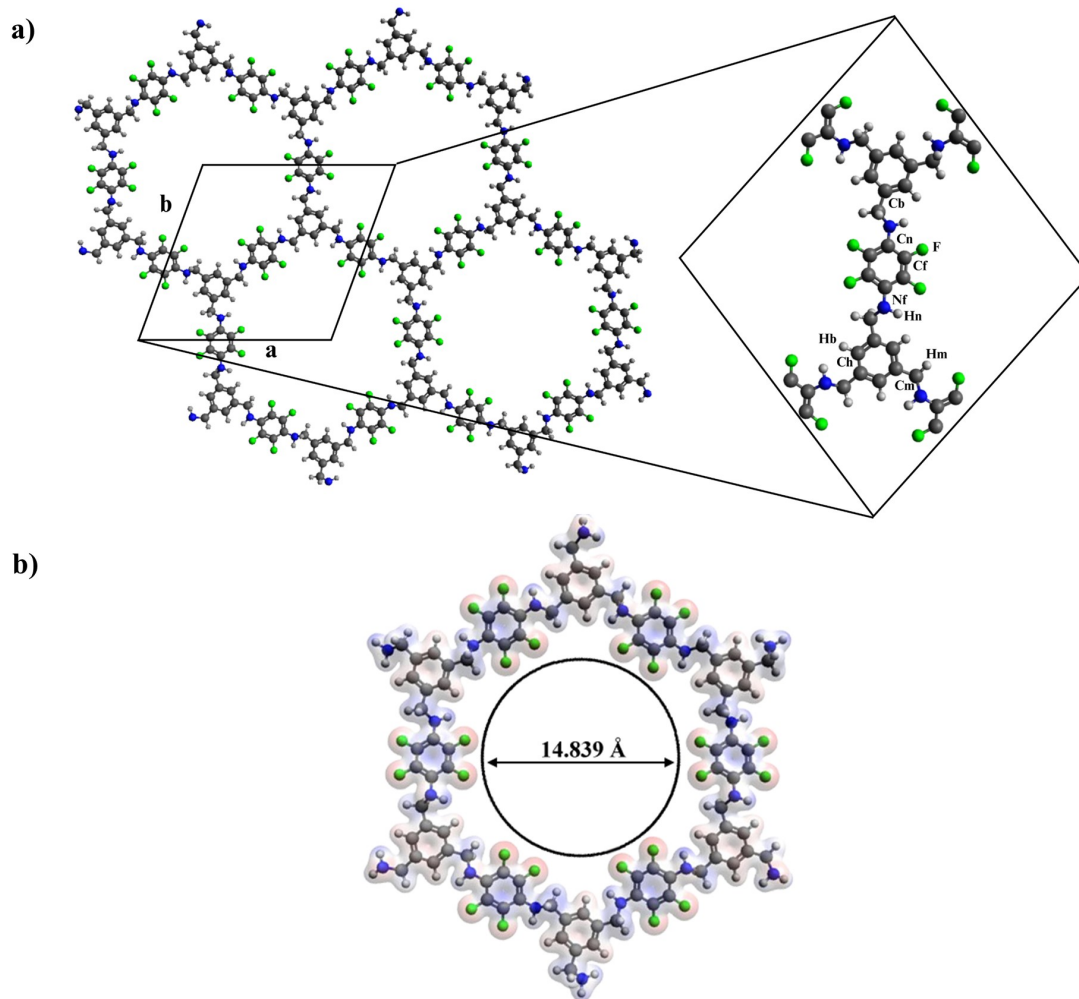


Figure 2. IPB-2F2 Represented by Its Hexagonal Lattice Structure Used in The Periodic DFT Relaxations Along with Its Atomic Labelling (a). A Unit Pore of IPB-2F2 Represented by The Electron Density (Iso-Value = 0.02 E Bohr^{-3}) (b)

manifested in the corresponding adsorption isotherm. The relationship between the amount of adsorbed gas on the membrane surface and the gas pressure at a constant temperature, the adsorption isotherm, can be used to explain adsorption phenomenon (Lee et al., 2021). IPB-2F2 exhibited a higher adsorption isotherm curve for CO_2 and N_2 gases than IPB-2H, indicating that IPB-2F2 can adsorb more gas molecules. The linear relationship between pressure and the amount of gas adsorbed further confirms the enhanced adsorption capacity of IPB-2F2. We also found that CO_2 gas tended to be adsorbed near the fluorine atoms of the IPB-2F2 membrane, as the fluorine atoms continuously attracted CO_2 molecules. As illustrated in Figure 5, the gas density plotted along the z -axis demonstrated that the amount of adsorbed CO_2 increases proportionally with pressure. Indeed, higher pressures lead to a greater probability of CO_2 adsorption on the IPB-2F2 membrane.

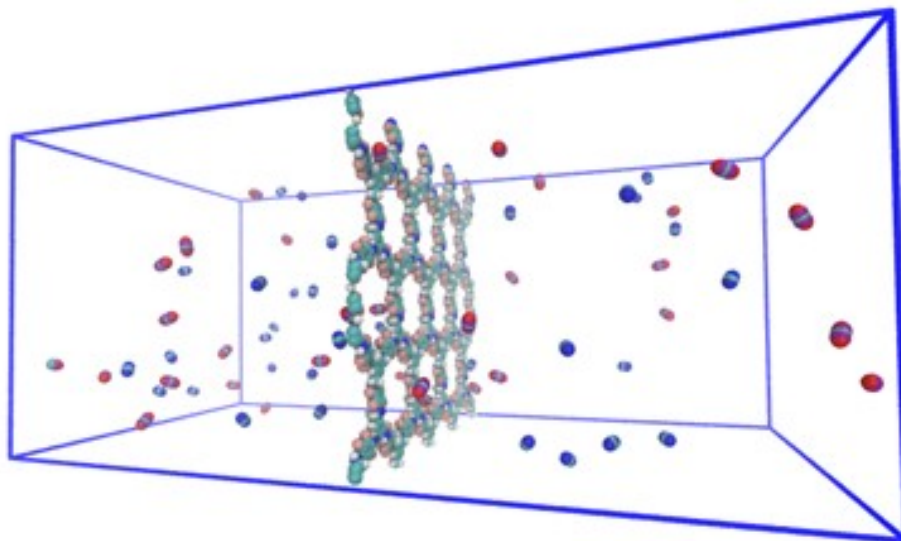
The gas adsorption on the IPB-2F2 surface is driven by in-

termolecular interactions comprising both electrostatic and van der Waals contributions. Table 2 presents the van der Waals and Coulombic (electrostatic) energy components obtained from molecular dynamics (MD) simulations, clearly demonstrating that electrostatic interactions dominate the overall energy profile. This dominance is expected due to the long-range nature of Coulombic interactions, emphasizing the importance of accurately determining partial atomic charges. In contrast, van der Waals interactions contribute minimally to the total interaction energy. However, upon closer inspection of Table 2, the observed differences between systems at varying pressures are primarily attributed to van der Waals forces. While Coulombic energies remain consistent across different pressures, van der Waals interactions differentiate the systems, indicating that increased pressure enhances CO_2 adsorption on IPB-2F2 due to the influence of van der Waals forces (Figures 4 and 5). Consequently, the application of an improved Lennard-Jones potential is critical to accurately model these

Table 1. The Optimized Structural Parameters of IPB-2F2 in Terms of Bond Radius (Å) and Bond Angle (°) in Comparison with Other Structures in Existing Literatures

Parameters	IPB-2F2	IPB-2H ^[1]	CTF-0 ^[2]	Benzoimidazole-Based Hydrazones ^[3]	BND-TFB ^[4]
r Cf-F	1.36	-	-	1.35	-
r Cn-N	1.40	1.40	-	-	-
r Cf-Cn (cyclic)	1.40	1.41	1.40	1.40	-
r Cn-Cf (cyclic)	1.41	1.41	1.40	1.40	-
r Cf-Cf	1.39	1.41	1.40	1.40	-
r Cb-Cm ($sp^2 - sp^3$)	1.51	1.51	1.48	1.51	-
r Cb-Ch (cyclic)	1.40	1.41	1.40	1.40	-
r Cm-Nf	1.47	1.45	-	-	-
∠Cb-Ch-Cb	121.30	121.40	-	-	120.70
∠Ch-Cb-Ch	118.80	118.70	-	-	119.30
∠Cb-Cm-Nf	114.10	114.50	-	-	-
∠Ch-Cb-Cm	122.90	123.90	-	-	121.40
∠Cb-Ch-Hb	120.60	121.00	-	-	120.20
∠Cm-Nf-Hn	112.70	114.10	-	-	-
∠Cm-Nf-Cn	117.10	119.90	-	-	-
∠Cn-Cf-Cf	122.20	121.10	-	-	120.50
∠Cf-Cn-Cf	115.40	117.50	-	-	118.70
∠Cn-Cf-F	118.40	-	-	-	-

Source: ^[1]Apriyanto et al. (2020), ^[2]Wang et al. (2016), ^[3]Rafiq et al. (2019), ^[4]Vitaku and Dichtel (2017)

**Figure 3.** Snapshot of The Simulation Box at P = 2.54 atm. N₂ Molecules are Colored Blue, While CO₂ Molecules are Colored Cyan and Red

short-range interactions compared to the standard Lennard-Jones potential.

Furthermore, the diffusion and adsorption coefficients for IPB-2F2 were compared with those of IPB-2H (Table 3). The diffusion coefficient, defined as the rate of gas movement through the membrane, was lower for IPB-2F2 under the same pressure conditions suggesting that the stronger attraction due

to fluorine addition inhibited gas diffusion. Moreover, the diffusion coefficient decreased with increasing pressure, indicating that a greater number of gas molecules could impede the movement of other molecules through the membrane. Conversely, the adsorption coefficient, derived from the slope of the adsorption isotherm curve, was higher for IPB-2F2 than for IPB-2H. This suggests that IPB-2F2 absorbs more gas molecules, at-

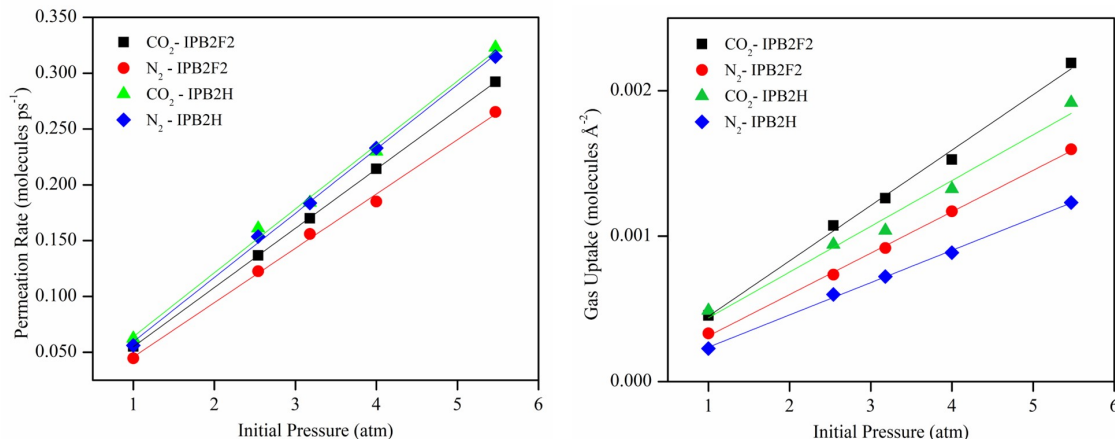


Figure 4. Permeation Rate as a Function of Initial Pressure (Left Panel) and Adsorption Isotherms (Right Panel) of IPB-2F2 and IPB-2H at 353 K

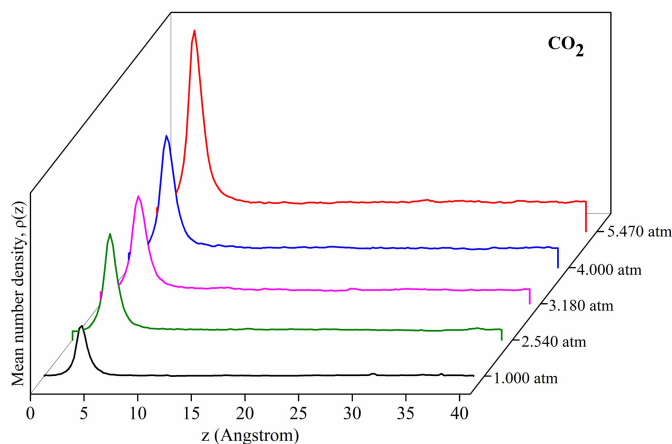


Figure 5. The z -density Profiles of CO₂ Adsorption from the IPB-2F2 Surface

tributed to weak intermolecular forces such as van der Waals interactions between fluorine atoms and CO₂ molecules. It was reported that the C–F bond's longer length (0.1332 nm) and greater strength (111 kcal mol⁻¹) compared to C–H bonds, along with its strong polarity, further enhanced CO₂ adsorption (Yu et al., 2012).

Adsorption selectivity parameter was calculated based on Equation (1). The selectivity results showed that the CO₂/N₂ gas selectivity of IPB-2F2 was not significantly different from that of IPB-2H (Table 4). This indicates that the IPB-2F2 membrane absorbs both CO₂ and N₂ strongly. The adsorption isotherm curve also showed an increase in the number of adsorbed gas molecules for both gases. This finding contrasts with the work of Zhao et al. (2013), who reported increased CO₂ selectivity in fluorinated Covalent Triazine-based Frameworks (F-CTF) due to multilayer membrane structures. Tong et al. (2016) also noted that overlapped CTF-1 membranes exhibit

Table 2. The van der Waals and Coulomb Energies Measured During the MD Simulations

P (atm)	van der Waals (kcal mol ⁻¹)	Coulomb (kcal mol ⁻¹)
1.000	-4.870 ± 4.327	-206.460 ± 0.303
2.540	-9.755 ± 3.654	-206.590 ± 0.456
3.180	-10.861 ± 3.553	-206.640 ± 0.496
4.000	-13.316 ± 4.156	-206.690 ± 0.549
5.470	-20.010 ± 4.805	-206.950 ± 0.706

higher selectivity than single-layer membranes, a phenomenon similarly reported Apriliyanto et al. (2022) for graphtriene membranes with trilayer structures showing the highest selectivity. It is important to note that in this study, IPB-2F2 was examined in its monolayer form, and different adsorption behaviors may be observed with multilayer membranes.

Despite the adsorption selectivity of IPB-2F2 is lower than IPB-2H, the selectivity value of IPB-2F2 remained greater than 1, indicating that the membrane is selective for CO₂ with CO₂ molecules more readily adsorbed on the membrane surface than N₂. These selectivity results are comparable with other 2D materials in its monolayer form reported in Table 4. The IPB-2F2 is even better than those reported by Tong et al. (2016) and Goethem et al. (2024), where the CTF-1 membrane and NPC film are not selective by only showing a selectivity of 0.89 and 0.90, respectively. Additionally, structural modification by adding fluorine atoms can make the membrane more hydrophobic, suggesting its potential application in industrial flue gases where it may resist the influence of water vapor Ozdemir et al. (2019).

$$S_{ads}^{CO_2/N_2} = \frac{n_{CO_2 ads}}{n_{CO_2 free}} \times \frac{n_{N_2 free}}{n_{N_2 ads}} \quad (1)$$

Table 3. Diffusion and Adsorption Coefficients for CO₂/N₂ Mixture Systems at 353 K

Coefficient	P (atm)	IPB-2F2		IPB-2H ^[1]	
		CO ₂	N ₂	CO ₂	N ₂
Diffusion ($\times 10^{-6} \text{ m}^2 \text{ s}^{-1}$)	1.000	1.857	2.077	2.162	4.236
	2.540	2.833	2.792	3.030	3.592
	3.180	1.814	1.561	2.003	3.155
	4.000	1.625	2.010	1.962	2.569
	5.470	1.677	2.583	1.781	2.233
Adsorption (molecule $\text{Å}^{-2} \text{ atm}^{-1}$)		3.81×10^{-4}	2.85×10^{-4}	3.14×10^{-4}	2.22×10^{-4}

Source: ^[1]Apriliyanto et al. (2020)**Table 4.** Comparison of CO₂/N₂ Selectivity Between IPB-2F2 and Other 2D Materials in Existing Literatures

Materials	System's condition	Selectivity	Ref.
IPB-2F2	1.00; 2.54; 3.18; 4.00; 5.47 atm & 353 K	1.48; 1.58; 1.46; 1.37; 1.46	This work
IPB-2H	1.00; 2.54; 3.18; 4.00; 5.47 atm & 353 K	2.53; 1.71; 1.52; 1.59; 1.67	Apriliyanto et al. (2020)
Nanoporous carbon (NPC) film	1.97 atm & 308 K	0.90	Goethem et al. (2024)
g-C10N9 membrane	298 K (pressure not specified)	1.00	Chang et al. (2018)
Bilayer graphene oxide (GO) sheets (W2, D = 9 Å)	127.71 atm & 298 K	1.00	Wang et al. (2017)
Graphdiyne-like monolayers (GDY_H; GDY_F)	2.96 atm & 298 K	1.10; 1.70	Zhao et al. (2017)
Valent triazine-based frameworks (CTF-1)	9.87 atm & 300 K	0.89	Tong et al. (2016)
Squaraine-bridged COFs (SQ-COPs-2/3)	< 9.87 atm & 298 K	1.50	Huang and Cao (2016)
Graphene oxide (GO) membrane (8.3 Å spacing)	298 K (pressure not specified)	1.00-1.30	Li et al. (2016)
Fluorine-modified porous graphene	300 K (pressure not specified)	1.69	Wu et al. (2014)

4. CONCLUSIONS

The effects of fluorine substitution in diamine COF (IPB-2F2) performance on CO₂/N₂ adsorption and separation have been investigated through computational analysis by means of DFT calculations and MD simulations. Structural optimizations results revealed a reduced pore size for IPB-2F2 in comparison with IPB-2H due to fluorine's large atomic size and high electronegativity. MD simulations showed that IPB-2F2 had lower CO₂ and N₂ permeation rates than IPB-2H, indicating that fluorine atoms reduced gas permeation. Adsorption isotherms demonstrated that fluorine substitution enhanced gas uptake capacities of COF. From an energetical point of view, gas adsorption on the surface of COFs was mainly governed by the van der Waals interactions. Therefore, substituting hydrogen with fluorine atoms that had higher polarizability increased gas adsorption by magnifying the dispersion forces (a main com-

ponent of van der Waals forces). Selectivity analysis indicated that IPB-2F2 preferentially adsorbs CO₂ over N₂, with adsorption selectivity values consistently greater than 1. Finally, the enhanced hydrophobicity of IPB-2F2 suggests suitability for industrial applications as CO₂ capture material, where the post-combustion flue gas contains water vapor.

5. ACKNOWLEDGMENT

We would like to express our gratitude for the research funding provided by the Indonesian Endowment Fund for Education (LPDP) through the Equity Program (DAPT), specifically under the national research collaboration scheme/Riset Kolaborasi Nasional (Ri-Na) under contract number 525/IT3.D10/PT.01.03/P/B/2023.

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