

## Layered Double Hydroxide/C (C=Humic Acid;Hydrochar) As Adsorbents of Cr(VI)

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### Abstract

Layered double hydroxide (LDH) is known as a layered material that can be used as an adsorbent to remove pollutants from aqueous solutions. The use of layered double hydroxide as an adsorbent is not very effective due to its structure which is easily damaged so that it cannot be reused and its small surface area which results in a small adsorption capacity. This can be overcome by developing layered double hydroxide into a composite material. Modification of layered double hydroxide is done by using supporting materials in the form of humic acid and hydrochar. In this study the adsorbent was applied in the removal of Cr(VI) metal from aqueous solutions. The layered double hydroxide modification process was successfully carried out as seen from the XRD, FTIR, and BET analysis. XRD analysis shows the peaks that appear in Mg/Al-AH and Mg/Al-HC are peaks composed of their constituent materials, namely Mg/Al LDH, humic acid, and hydrochar. The vibrations that appear in Mg/Al-AH and Mg/Al-HC are vibrations originating from Mg/Al, humic acid, and hydrochar. The layered double hydroxide material composited with humic acid showed a surface area from 2.155 m<sup>2</sup>/g to 3.337 m<sup>2</sup>/g. The layered double hydroxide material composited with hydrochar showed a larger surface area than the Mg/Al LDH base material. The surface area increased 37 times, from 2.155 m<sup>2</sup>/g to 74.207 m<sup>2</sup>/g. The Mg/Al-AH composite showed the first adsorption ability of 89.064% and there was no significant decrease in the next cycle. The Mg/Al-HC composite showed adsorption ability in the first cycle which reached 97.079%, the ability to survive up to the fifth cycle with a final ability of 75.029%.

### Keywords

Composite, Layered Double Hydroxide, Humic Acid, Hydrochar, Adsorption

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### 1. INTRODUCTION

The chemical, paper, and pharmaceutical industries are considered to be the main sources of heavy metal pollution in the environment. Pollution can cause problems in human health and ecosystems (Ahmadpoor et al., 2019). The problem of heavy metal pollution has high toxicity and cannot be decomposed naturally (Chen et al., 2019). Thus, a method is needed to reduce metal content in waste. Various methods have been carried out to reduce heavy metal levels from waste such as oxidation (El-Sherif et al., 2013), coagulation (Huang et al., 2019), ion exchange (Shrestha, 2018), and adsorption (Shrestha, 2018). Among these methods, adsorption is a method that has high efficiency and low cost and flexibility and simple operation (Gadekar and Ahammed, 2016). Raw materials that can be used as adsorbents in the Cr(VI) adsorption process include activated carbon (Li et al., 2020b), chitosan (Hasan et al., 2020), graphene (Hosseinzadeh and Ramin,

2018), biochar (Zubair et al., 2021), banana peels (Shrestha, 2018), and layered double hydroxide (Hatami et al., 2018).

Layered double hydroxide (LDH) known as hydrotalcite clay or anionic clay, has attracted attention in various fields such as catalysts, hydrogenation, oxidation, ion exchange, and adsorption (Hu et al., 2020). LDH is an efficient material to absorb/remove heavy metals from aqueous solutions (Rahmanian et al., 2018). LDH is a layered material with a layer such as positively charged brucite which has the general formula  $[M^{2+}_{1-x}M^{3+}_x(OH)_2]^{x+}(A^{n-})_{x/n}\cdot mH_2O$  where  $M^{2+}$  and  $M^{3+}$  denote metal ions located on the sheet the positively charged octahedral (Marques et al., 2020).  $M^{2+}$  is a divalent metal ion and  $M^{3+}$  is a trivalent metal ion.  $A^{n-}$  is an interlayer anion that can be exchanged to neutralize positive charges,  $x$  ranges from 0.17 to 0.33 and  $x$  is the molar ratio (Mahjoubi et al., 2017).

The characteristics of LDH have flexible properties that are easy to modify and have interlayer anions that are easily

exchanged but the stability of the structure is poor. LDH can be peeled off during the application process so that it can be reused very rarely and the LDH structure is more stable (Siregar et al., 2021). Therefore, it is necessary to improve the layered double hydroxide structure in order to strengthen the structure by inserting the support material. Supporting materials that can be used include biochar (Bolbol et al., 2019), hydrochar (Zhang et al., 2014), graphene (Siregar et al., 2021), chitosan (Saheed et al., 2020), and humic acid (Li et al., 2020a). The supporting material has active sites such as OH, COOH, NH<sub>2</sub> so that it has the potential as a supporting material in the modification process.

Lee et al. (2019) in their research used Mg/Al-biochar for phosphate adsorption with an adsorption capacity of 70.75 mg/g. Research conducted by Zhang et al. (2020) using Mg/Al intercalated diethyldithiocarbamate as a Cr(VI) adsorbent resulted in an adsorption capacity of 52.00 mg/g. Another layered double hydroxide use is Cu/Al modified using biochar from rice husk with increased adsorption capacity from 22.272 mg/g to 384.615 mg/g (Palapa et al., 2021).

In this study, the synthesis material of Mg/Al-AH and Mg/Al-HC from humic acid and hydrochar from *Lansium domesticum* peel was used to adsorb Cr(VI) metal. The effect of concentration variation and temperature variation of adsorption and desorption studies were tested using several solvents which aimed to determine the solvent with optimum Cr(VI) desorption conditions and the regeneration study was carried out in five cycles.

## 2. EXPERIMENTAL SECTION

### 2.1 Materials and Method

The chemicals used in this experiment Mg(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O (Merck, 256.41 g/mol), Al(NO<sub>3</sub>)<sub>2</sub>.9H<sub>2</sub>O (Merck, 375.13 g/mol), NaOH (Merck, 40.00 g/mol), HCl 37% by MallinckrodtAR, C<sub>2</sub>H<sub>5</sub>OH (Avantor, 99%), the humic acid by Merck extracted from the peat soil as shown in Figure 1, the hydrochar source was made from *Lansium domesticum* peel. Water was obtained using Purite water purification system from the Research Center of Inorganic Materials and Complexes. The material characterization was performed using XRD Rigaku Miniflex-6000. FTIR analysis was conducted using Shimadzu FTIR Prestige-21 by the KBr method and was scanned at 400-4000 cm<sup>-1</sup>. Adsorption-desorption of N<sub>2</sub> Analysis was measured using Quantachrome Micrometric ASAP. The concentration of the dye was analyzed using spectrophotometer UV-Visible Biobase BK-UV 1800PC.

### 2.2 Preparation of Mg/Al LDH (Chen et al., 2017)

Mg(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O and Al(NO<sub>3</sub>)<sub>2</sub>.9H<sub>2</sub>O at Mg<sup>2+</sup>/Al<sup>3+</sup> with molar ratio of 3:1 were weight and dissolved in purification water (called Mg/Al solution). The NaOH added slowly into Mg/Al solution until pH value achieved to 10. After the addition was complete, the mixture was stirred for 1 hour, followed by increasing the temperature at 65°C for 6 hours. The prod-



Figure 1. Humic Acid Extraction from Peat Soil

uct obtained is then filtered, washed until neutral and dried. Then, the material obtained is called Mg/Al-LDH.

### 2.3 Preparation of Hydrochar from *Lansium Domesticum* Peel by Hydrothermal Carbonization Method

The preparation of the hydrochar material was carried out using 2.5 g of mashed *Lansium domesticum* peel as shown in Figure 2 and then put into a hydrothermal stainless-steel autoclave and added 50 mL of distilled water. Then put in the oven at 200°C for 12 hours. Then the obtained material is cooled and dried in an oven at a temperature of 100°C.



Figure 2. Preparation of Hydrochar from *Lansium Domesticum* Peel by Hydrothermal

### 2.4 Preparation of Mg/Al-AH (Rahmadan et al., 2021)

The preparation of Mg/Al-AH material is the same as the preparation of Mg/Al-HC using the coprecipitation method with the following procedure 30 mL of Mg(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O 0.75 M mixed with 30 mL of Al(NO<sub>3</sub>)<sub>2</sub>.9H<sub>2</sub>O 0.25 M. Then NaOH 2 M is added dropwise drops to pH 10 and added 3 g of humic acid powder. The suspension was stirred at 80°C for 3 days. The product obtained is then filtered, washed until neutral and dried.

### 2.5 Preparation of Mg/Al-HC (Normah et al., 2021)

The Mg/Al-HC material was prepared using the coprecipitation method. As much as 30 mL Mg(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O 0.75 M mixed with 30 mL Al(NO<sub>3</sub>)<sub>2</sub>.9H<sub>2</sub>O 0.25 M. then, NaOH was added dropwise to reach pH 10. Afterwards, as much as 3 g of hydrochar of *Lansium domesticum* peel was added to the mixture. The mixture was stirred at a temperature of 80°C for 3 days. The product obtained is then filtered, washed until neutral and dried.

### 2.6 Adsorption Process

Isotherms and thermodynamic parameters are determined by concentration variation of (50, 60, 70, 80, 90, dan 100) mg/L

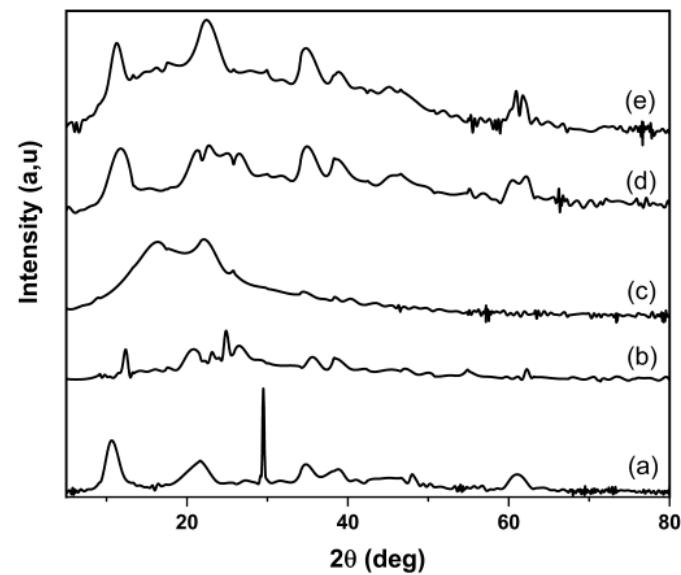
as much as 20 mL, added 0.02 g of adsorbent and temperature variations at 30-60°C. The concentration of Cr(VI) was analyzed after complexing using diphenylcarbazide at a wavelength of 543 nm.

## 2.7 Regeneration

As much as 5 g of adsorbent was put in 50 mL of 100 mg/L Cr(VI) and then stirred for 2 hours. After that, the centrifugation process is carried out to separate the adsorbent and the adsorbate residue. The solution was measured using a UV-Vis spectrophotometer after being complexed with diphenylcarbazide and the adsorbent was dried for desorption using water. The regeneration process is carried out by the adsorption-desorption process repeatedly in 5 cycles.

## 3. RESULTS AND DISCUSSION

Figure 3 shows the XRD pattern of each adsorbent. Figure 3(a) is an XRD pattern of Mg/Al showing the appearance of a typical layered double hydroxide peak at  $2\theta$  angles 11.47°(003), 22.86°(006), 61.62°(113), 65.50°(116) according to JCPDS data No. 22-700 where the Mg/Al diffraction pattern appears at 11.8°(003), 23.6°(006), 62.3°(113) and 66.3°(116). Research conducted by Chen et al. (2017) said that the diffraction peak around an angle of 11°(003) with high intensity in Mg/Al indicated the success of the synthesis of LDH materials.

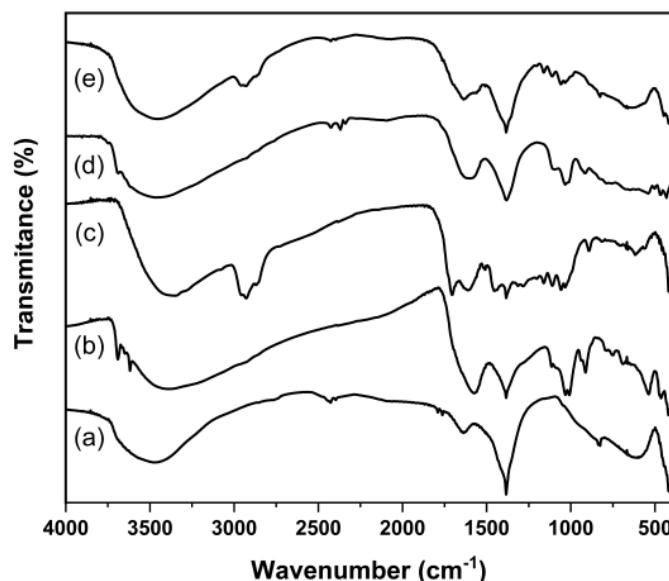


**Figure 3.** XRD Powder Patterns of Mg/Al LDH (a), AH (b), HC (c), Mg/Al-AH (d), and Mg/Al-HC (e)

Then the Mg/Al LDH material was modified using humic acid and hydrochar to form a composite. The modification process aims to obtain materials that have a larger surface area so that the adsorption capacity increases and the material structure is more stable so that it can be used repeatedly. The humic acid used was derived by Merck, and hydrochar obtained from the

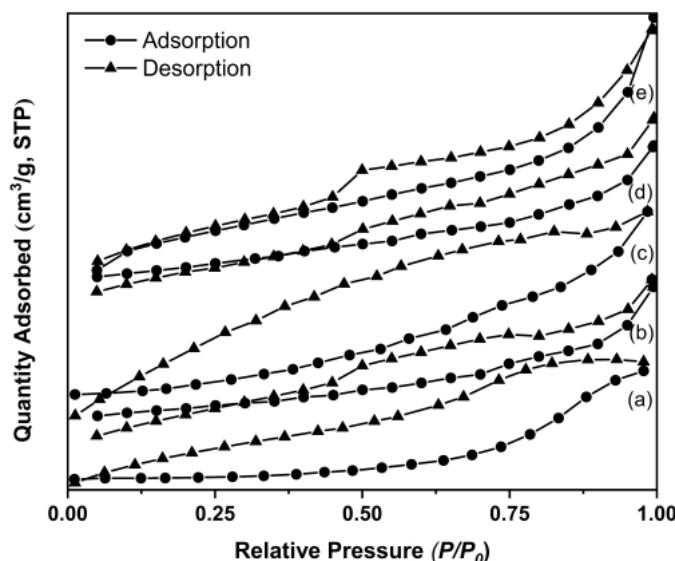
carbonization process of *Lansium domesticum* peel using the hydrothermal method. The obtained humic acid and hydrochar were characterized using XRD analysis.

Figure 3(b) shows the XRD pattern of humic acid. The XRD pattern of humic acid shows that diffraction peaks appear at angles of 20.01°(006), 24.88°(006) and 26.4°(006). According to Zhang et al. (2018) strong diffraction peaks that appear at angles of about 21°, 26.7°, 31.48° indicate the presence of large amounts of carbon contained in humic acid and has a fairly high crystallinity. The XRD pattern of the hydrochar shown in Figure 3(c) shows that peaks appear at an angle of  $2\theta$ , namely 16°(003) and 22.47°(006). The diffraction peak of hydrochar at an angle of 16°(003) has a lower intensity than the peak at an angle of 22.47°(006) indicating of cellulose.



**Figure 4.** FTIR Spectrum of Mg/Al LDH (a), AH (b), HC (c), Mg/Al-AH (d), and Mg/Al-HC (e)

The Mg/Al-AH diffraction peaks are shown in Figure 3(d). Figure 3(d) shows peaks appearing at the diffraction angles of 11.65°(003), 21°(006), 24°(006), 31.05°(012), 39.2°(015) and 61.5°(110). The diffraction peaks that appear at angles of 11.65° and 61.5° are characteristic of Mg/Al LDH which indicates a layered structure, while the diffraction peaks that appear at angles of about 21°(006), 26°(006) and 31.05°(012) are characteristics of humic acid materials that have a large amount of carbon content tall one. This indicates that the preparation of Mg/Al-AH composite was successful. Figure 3(e) shows the XRD pattern of Mg/Al-HC with diffraction angles at 11.22°(003), 11.6°(003), and 61°(110). The peak that appears is the peak of the base material in the form of Mg/Al and the supporting material in the form of hydrochar. This is in accordance with the notion of composites, namely materials obtained from a combination of two or more materials with different characteristics, in order to obtain better characteristics



**Figure 5.** BET Profile of Mg/Al LDH (a), AH (b), HC (c), Mg/Al-AH (d), and Mg/Al-HC (e)

than the constituent materials.

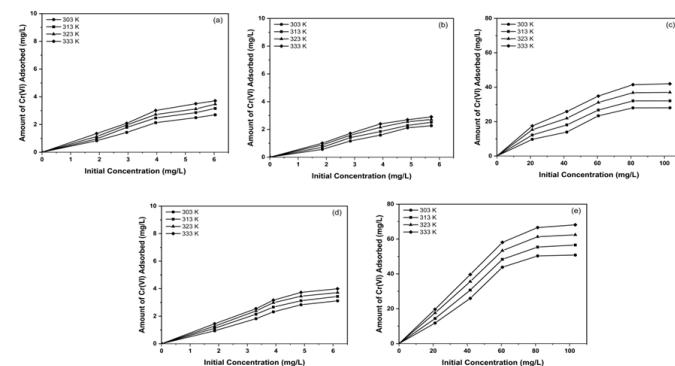
Figure 4 shows the spectra of each material. Figure 4(a) is a spectrum of Mg/Al LDH where a vibration peak appears at a wave number of  $3500\text{ cm}^{-1}$  which indicates -OH vibrations from water molecules, and vibrations at  $1635\text{ cm}^{-1}$  which indicate stretching vibrations from -OH. There is also a vibration at  $1381\text{ cm}^{-1}$  which indicates the presence of an N-O group derived from nitrate. The small peak that appears at the wave number of  $748\text{ cm}^{-1}$  is the M-O vibration in the form of Mg-O and Al-O (Zhang et al., 2018). Figure 4(b) shows the FTIR spectrum of humic acid. The wide vibrational peak at the wave number  $3300\text{-}3500\text{ cm}^{-1}$  indicates the presence of an -OH group. The peak of the vibration at the wave number  $1530\text{-}1570\text{ cm}^{-1}$  indicates the presence of an aromatic C=C stretching vibration. The vibration peaks produced from the wave number  $1375\text{-}1390\text{ cm}^{-1}$  indicate the presence of C-H bending vibrations and C-H deformation of the aromatic  $\text{CH}_2$  and  $\text{CH}_3$  groups, while the peak vibrations at the wave number  $1010\text{-}1050\text{ cm}^{-1}$  indicate the presence of C-O stretching vibrations of the polysaccharides. According to Helal et al. (2011) the FTIR spectrum of humic acids which shows the dominance of the OH, COOH and  $\text{COO}^-$  groups is a characteristic of humic soils. Hydrochar spectrum appears at wave numbers  $3425\text{ cm}^{-1}$  and  $1625\text{ cm}^{-1}$  which is the -OH vibration of the water molecule and the strain vibration of -OH. In addition, a vibration appears at wave number  $2931\text{ cm}^{-1}$  which is a -CH stretching vibration of the lignin contained in the hydrochar as shown in Figure 4(c).

The Mg/Al-AH spectrum is shown in Figure 4(d), peak appears at a wave number of  $1381.03\text{ cm}^{-1}$  which indicates the presence of nitrate bonding vibrations, thus illustrating the presence of nitrate anions in Mg/Al and a peak at a wave

number of  $432.05\text{ cm}^{-1}$  and  $540.07\text{ cm}^{-1}$  which indicate the buckling vibrations of Mg-O and Al-O. Another vibration that appears is at wave number  $3464.15\text{ cm}^{-1}$  which is marked by a wide peak which indicates the O-H stretching vibration. In addition, there is a vibration peak at wave number  $1604.77\text{ cm}^{-1}$  which indicates the presence of a C=C group from the aromatic ring or conjugated H from the C=O group from the carbonyl group (carboxylate or ketone). The FT-IR spectrum of Mg/Al-HC shown in Figure 4(e) shows that there is a vibration resembling Mg/Al LDH as its constituent material and a vibration appears at a wave number of  $1931\text{ cm}^{-1}$  which indicates the presence of C=O vibrations from the supporting material in the form of hydrochar (Normah et al., 2021).

The adsorption-desorption isotherm pattern of each material is shown in Figure 5. Figure 5 shows the pattern of each material following a type IV isotherm pattern and a hysteresis loop type 3 where the adsorption-desorption patterns do not overlap and the pores are not uniform. The type IV isotherm pattern indicates a mesoporous material (Palapa et al., 2021). The nitrogen desorption adsorption pattern in Figure 5 produces the values of the surface area, pore volume, and pore diameter of each material as presented in Table 1.

Table 1 shows the basic material Mg/Al LDH has a surface area of  $2.155\text{ m}^2/\text{g}$ , and the supporting material for humic acid and hydrochar is  $2.750\text{ m}^2/\text{g}$  and  $22.635\text{ m}^2/\text{g}$ , respectively. The process of modifying layered double hydroxide into composites has succeeded in increasing the surface area of Mg/Al LDH. The layered double hydroxide material composited with humic acid showed a surface area from  $2.155\text{ m}^2/\text{g}$  to  $3.337\text{ m}^2/\text{g}$ . The layered double hydroxide material composited with hydrochar showed a larger surface area than the Mg/Al LDH base material. The surface area increased 37 times, from  $2.155\text{ m}^2/\text{g}$  to  $74.207\text{ m}^2/\text{g}$ . Hydrochar using the hydrothermal carbonization method while humic acid does not, so the carbon that is still joined in the hydrochar is hydrolyzed so that the surface area of Mg/Al-HC is larger than that of Mg/Al-AH.



**Figure 6.** Effect of Adsorption Contact Time on Mg/Al LDH (a), AH (b), HC (c), Mg/Al-AH (d), and Mg/Al-HC (e)

Figure 6 shows that as the temperature increases, more Cr(VI) is adsorbed. The maximum adsorption process of

**Table 1.** BET Analysis of Materials

Adsorbent	Surface Area (m <sup>2</sup> /g)	Pore Volume (cm <sup>3</sup> /g) BJH	Pore Size (nm), BJH
Mg/Al LDH	2.155	0.028	6.225
AH	2.75	0.028	6.223
HC	22.635	0.044	2.769
Mg/Al-AH	3.387	0.007	4.165
Mg/Al-HC	74.207	0.148	19.102

**Table 2.** Isotherm Adsorption

Adsorbent	Adsorption Isotherm	Adsorption Constant	T (K)			
			303	313	323	333
MgAl/ LDH	Langmuir	$Q_{max}$	30.211	28.736	27.933	28.09
		$K_L$	0.074	0.113	0.191	0.279
		$R^2$	0.997	0.999	0.999	0.999
	Freundlich	$n$	0.624	0.748	0.431	0.81
		$K_F$	16.765	16.924	19.342	21.237
		$R^2$	0.981	0.981	0.953	0.993
AH	Langmuir	$Q_{max}$	3.509	13.643	21.368	9.634
		$K_L$	0.126	0.053	0.055	0.172
		$R^2$	0.926	0.987	0.935	0.806
	Freundlich	$n$	0.718	0.882	0.845	0.93
		$K_F$	0.469	0.755	1.093	1.392
		$R^2$	0.825	0.855	0.941	0.999
HC	Langmuir	$Q_{max}$	34.364	45.662	46.083	48.78
		$K_L$	0.028	0.037	0.066	0.105
		$R^2$	0.977	0.94	0.967	0.982
	Freundlich	$n$	0.599	0.967	0.51	0.602
		$K_F$	2.086	4.024	7.463	11.256
		$R^2$	0.911	0.944	0.947	0.964
Mg/Al-AH	Langmuir	$Q_{max}$	32.017	9.804	6.969	6.072
		$K_L$	0.03	0.228	0.545	1.026
		$R^2$	0.91	0.951	0.941	0.95
	Freundlich	$n$	0.979	0.203	0.454	0.696
		$K_F$	1.196	1.781	2.404	2.998
		$R^2$	0.979	0.906	0.986	0.925
Mg/Al-HC	Langmuir	$Q_{max}$	208.333	86.957	74.627	78.74
		$K_L$	0.007	0.048	0.149	0.469
		$R^2$	0.998	0.999	0.956	0.993
	Freundlich	$n$	0.836	0.537	0.471	0.27
		$K_F$	1.153	2.563	8.547	9.707
		$R^2$	0.986	0.951	0.926	0.802

Cr(VI) occurs at a temperature of 333K.

The effect of adsorption isotherm and thermodynamics can be calculated through equation 5-8 according to (Siregar et al., 2021). The parameter  $Q_m$  is a constant that indicates the adsorbed solute at equilibrium or indicates monolayer adsorption.  $Q_m$  is the maximum adsorption capacity of an adsorbent with units of mg/g. While  $K_L$  is a constant that shows the

bond energy between the adsorbate and adsorbent (L/mg). The adsorption coefficient ( $K_F$ ) can be used as an indicator of adsorption capacity and  $1/n$  is the adsorption intensity. The higher the  $K_F$  value, the greater the adsorption capacity,  $n$  is a measure of deviation from the linearity of adsorption which is generally used to determine the correctness of an adsorption. If the value of  $n = 1$  then the adsorption that occurs is linear. If

**Table 3.** Thermodynamic Adsorption

Adsorbent	T (K)	Q <sub>e</sub> (mg/g)	ΔH (kJ/mol)	ΔS (J/mol K)	ΔG (kJ/mol)
MgAl/LDH	303	2.698	18.879	0.061	0.462
	313	3.157			-0.146
	323	3.466			-0.754
	333	3.708			-1.362
	303	2.268		0.038	1.036
AH	313	2.512	12.643		0.653
	323	2.717			0.27
	333	2.907			-0.113
	303	9.715		0.16	0.554
HC	313	12.244	29.09		-1.048
	323	15.285			-2.65
	333	17.512			-4.252
	303	3.114		0.054	-0.059
Mg/Al-AH	313	3.434	16.423		-0.603
	323	3.716			-1.147
	333	3.993			-1.691
Mg/Al-HC	303	50.311	28.811	0.099	-1.124
	313	55.392			-2.112
	323	61.327			-3.1
	333	66.579			-4.088

the value of  $n < 1$  then the adsorption process is a chemical adsorption process, but if the value for  $n > 1$  then the adsorption is physical adsorption.

Changes in the concentration of adsorbate in the adsorption process can be studied through adsorption isotherms. The adsorption isotherms commonly used are Langmuir and Freundlich isotherms (Normah et al., 2021). Determination of the equilibrium model depends on the value of the determinant coefficient ( $R^2$ ) close to 1. The data in Table 2 shows that the adsorption process using Mg/Al LDH, AH, HC, Mg/Al-AH, and Mg/Al-HC tends to follow the Langmuir equation seen from  $R^2$  value is closer to 1. The Langmuir adsorption isotherm pattern indicates that the adsorption takes place only in one layer (monolayer) and the surface sites are homogeneous because each active site can only adsorb 1 molecule. Characteristics of chemical adsorption is that it occurs at high temperatures, the type of interaction is chemical interaction, and the process is irreversible. The maximum adsorption capacities of Mg/Al LDH, AH, HC, Mg/Al-AH, and Mg/Al-HC were 30.211 mg/g, 13.643 mg/g, 34.364 mg/g, 32.017 mg/g, and 208.333 mg/g as shown in Table 2. Based on the data obtained in Table 2, Mg/Al-AH and Mg/Al-HC have a greater adsorption capacity because the surface area is larger than the constituent material than the constituent materials so that they are more effectively used as adsorbents in the process of removing Cr(VI) metal from aqueous aqueous solutions.

Table 3 shows the effect of thermodynamics on adsorption. The determined thermodynamic parameters include enthalpy

( $\Delta H$ ), entropy ( $\Delta S$ ), and gibbs free energy ( $\Delta G$ ) which are presented in Table 3. The determination of the value of  $\Delta H$  in the Cr(VI) adsorption process was carried out to determine whether the adsorption process was endothermic or exothermic, as well as the tendency of physical and chemical adsorption processes through the  $\Delta H$  value. The determination of  $\Delta S$  was carried out to determine the mobility of the adsorbate during the adsorption process, while  $\Delta G$  was determined to determine the spontaneity of the adsorption process (Amin et al., 2020).

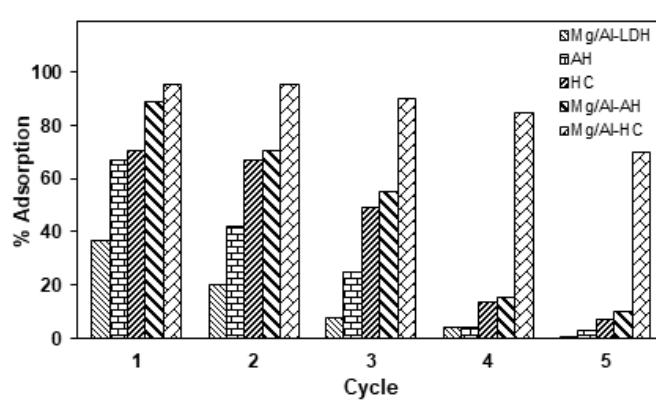
**Figure 7.** Regeneration of Mg/Al LDH, AH, HC, Mg/Al-AH, and Mg/Al-HC

Table 3 shows the positive  $\Delta H$  values. Siregar et al. (2021)

revealed that a positive value of  $\Delta H$  indicates that the adsorption process is endothermic, where the adsorbent and adsorbate require energy to interact with each other. The determination of  $\Delta S$  shows a small value indicating the degree of disorder during the adsorption process is small. The determination of the next thermodynamic parameter in the form of  $\Delta G$  is overall negative. This indicates that the adsorption process takes place spontaneously using little energy.

The regeneration process of Mg/Al-AH, and Mg/Al-HC composites are presented in Figure 7. Figure 7 shows the adsorption ability of Mg/Al-AH and Mg/Al-HC more stable than Mg/Al LDH, AH, and HC because Mg/Al-AH and Mg/Al-HC are protected by supporting materials in the form of humic acid and hydrochar. The Mg/Al-AH composite showed the first adsorption ability of 89.064% and there was no significant decrease in the next cycle. The Mg/Al-HC composite showed adsorption ability in the first cycle which reached 97.079% in the first cycle, the ability to survive up to the fifth cycle with a final ability of 75.029%.

#### 4. CONCLUSIONS

The preparation of Mg/Al composite with the supporting material in the form of humic acid and hydrochar has been successfully synthesized. This is evidenced from the results of the main characterization of XRD which shows the appearance of LDH peaks and the supporting material in the form of humic acid and hydrochar. The surface area of Mg/Al-AH and Mg/Al-HC is larger than the constituent materials, which are  $3.837 \text{ m}^2/\text{g}$  and  $74.207 \text{ m}^2/\text{g}$ , respectively. The maximum adsorption capacity of Mg/Al-AH and Mg/Al-HC is also greater than that of Mg/Al LDH, AH, and HC. The adsorption capacity of Mg/Al-AH was  $32.017 \text{ mg/g}$  and the adsorption capacity of Mg/Al-HC was  $208.333 \text{ mg/g}$ . The regeneration process is more effective using Mg/Al-AH and Mg/Al-HC as seen from the adsorption capacity which did not decrease significantly for five cycles.

#### 5. ACKNOWLEDGEMENT

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